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Fuel Unsaturation Effects on NOx and PAH Formation in Spray Flames

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5 Abstract

6 The effect of fuel unsaturation on NO_x and PAH formation in spray flames is investigated at diesel engine 7 conditions. The directed relation graph methodology is used to develop a reduced mechanism starting from the 8 detailed CRECK mechanism². The reduced mechanism and spray models are validated against the shock tube 9 ignition data and high-fidelity, non-reacting and reacting spray data from the Engine Combustion Network [26]. 10 3-D simulations are performed using the CONVERGE software to examine the structure and emission 11 characteristics of n-heptane and 1-heptane spray flames in a constant-volume combustion vessel. Results indicate 12 that the combustion under diesel engine conditions is characterized by a double-flame structure with a rich 13 premixed reaction zone (RPZ) near the flame stabilization region and a non-premixed reaction zone (NPZ) further 14 downstream. Most of NO_x is formed via thermal NO route in the NPZ, while PAH species are mainly formed in 15 the RPZ. A small amount of NO is also formed via prompt route in the RPZ, and via N₂O intermediate route in 16 the region outside NPZ, and via NNH intermediate route in the region between RPZ and NPZ. The presence of a 17 double bond leads to higher flame temperature and thus higher NO in 1-heptene flame than that in n-heptane 18 flame. It also leads to the increased formation of PAH species, implying increased soot emission in 1-heptene 19 flame than that in n-heptane flame. Reaction path analysis indicate that the increased formation of PAH species 20 can be attributed to the significantly higher amounts of 1,3-butadiene and allene formed due to β scission 21 reactions resulting from the presence of double bond in 1-heptene.

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23 Keywords: Fuel Unsaturation, NO_x and PAH emissions, N-heptane and 1-heptene spray flames, 3D simulations

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² http://creckmodeling.chem.polimi.it/index.php/current-version-kinetic-mechanisms/low-and-high-temperature-complete-mechanism.

25 **1. Introduction**

26 Liquid fuels used in propulsion and power generation applications are generally composed of a large 27 number of hydrocarbon compounds, with several containing one or more unsaturated C=C bonds. Numerous 28 recent studies have reported that the fuel reactivity and ignition behavior are strongly influenced by the degree of 29 unsaturation, i.e., the number and position of double bonds. Detailed kinetic models [1,2,3] have been developed 30 to examine the effects of the presence and position of double bonds on fuel reactivity and ignitability. 31 Experimental investigations have also been performed using shock tube [4,5,6], RCM [7,8,9], and flow reactor 32 [10]. An important finding from these studies is that the ignition delay time could increase significantly, 33 especially in the NTC (negative temperature coefficient) region, due to the presence of double bonds in the fuel 34 molecular structure. The fuel ignitability is also found to be strongly influenced by the length of the saturated 35 portion aside the double bond, with the longer alkyl chain yielding shorter ignition delay.

36 Engine experiments [11,12,13] using different biodiesel fuels have also reported longer ignition delays as 37 a consequence of unsaturated components in fuel composition. In addition, these and other engine experiments 38 [14, 15] with biodiesels have observed that due to the higher concentration of unsaturated components, some 39 biodiesels produce more PM and UHC compared to those containing smaller amount of unsaturated components. 40 In order to explain these trends in engine PM emission, fundamental investigations have been reported on the 41 formation of soot precursors during the combustion of unsaturated biodiesel components. Garner et al. [6] 42 observed from their shock tube experiments that 1-heptene (1-C7H14) produces more acetylene than does the n-43 heptane (n-C₇H₁₆) over intermediate temperatures, 1100-1600K. Garner and Brezinsky [16] and Garner et al. [17] 44 subsequently extended the study to the oxidation of methyl octanoate and methyl trans-2-octenoate, and observed 45 longer ignition delay and increased acetylene (C_2H_2) formation in the case of unsaturated methyl ester. Note that 46 acetylene provides a major route for soot particle surface growth [18, 19]. Sarathy at el. [20] conducted flame 47 experiments and observed that compared to methyl butanoate, its unsaturated counterpart, methyl crotonate 48 produces higher amount of acetylene, propyne $(1-C_3H_4)$, 1-butene $(1-C_4H_8)$, 1,3-butadiene $(1,3-C_4H_6)$, and 49 benzene (C_6H_6), indicating the potential of increased soot formation with unsaturated biodiesel fuels compared to

the saturated ones. Our previous studies [21,22] on n-heptane and 1-heptene partially premixed counterflow flames (PPFs) revealed that 1-heptene produces higher amounts of acetylene and benzene compared to the saturated fuel, n-heptane. Further analysis indicated that the dominant path for benzene formation involves the recombination of propargyl radicals (C_3H_3), and the presence of the double bond in 1-heptene provides a significant route for its production through the formation of allyl radical (C_3H_5). This path is not favored in the oxidation of n-heptane, as it decomposes directly to smaller alkyl radicals.

56 While the aforementioned studies have provided significant insight pertaining to fuel reactivity and 57 ignitability, relatively little research has been reported concerning the combustion and emission behavior of 58 unsaturated hydrocarbons in realistic flames. The present study examines the effect of the presence of a double 59 bond on NO_x and PAHs emissions in spray flames under diesel engine conditions. 3-D simulations are performed 60 for the fuel injection, ignition, combustion, and emission characteristics using saturated and unsaturated fuels, 61 namely n-heptane and 1-heptene, respectively. It extends our previous investigations [21, 22], which considered 62 quasi-1-D partially premixed flames in a counterflow configuration, to more realistic spray flames using the 63 Sandia constant volume reactor. This reactor has been extensively used at Sandia National Laboratories [23, 24, 64 25] to provide high-fidelity data for non-reacting and reacting sprays. The data can be downloaded from the 65 Engine Combustion Network (ECN) [26] website.

66 N-heptane and 1-heptane flames are simulated by developing a skeletal mechanism, by reducing it from 67 the detailed CRECK mechanism [27], using the Directed Relation Graph methodology with Error Propagation 68 and Sensitivity Analysis [28, 29]. The skeletal mechanism is validated using ignition delay measurements for n-69 heptane and 1-heptene. The fuel oxidation model is then combined with the PAH and NO_x models, and 70 predictions for the n-heptane non-reacting and reacting sprays are validated against the ECN experimental data 71 [26]. Simulations are then performed to characterize the effects of fuel unsaturation or double bond on NO_x and 72 PAH emissions in spray flames at temperatures and pressures relevant to engine operating conditions. The 73 dominant NO_x and PAH species formation regions in these flames are identified using the scatter plots of relevant species in ϕ -T space. Finally, a reaction path analysis is conducted to identify the dominant paths for the formation of PAH species in n-heptane and 1-heptene flames.

76 2. Computational Model

77 Simulations are performed using a commercial CFD code, CONVERGE [30, 31], which incorporates the 78 state-of-the-art models for spray injection, atomization and breakup, turbulence, droplet collision and coalescence, 79 spray-wall interaction, and vaporization. Since the details of these models have been described elsewhere, only a 80 brief description is provided here. The 3D computational model for two-phase reacting flow is based on an 81 Eulerian-Lagrangian formulation. Gas-phase flow field is described by the Favre-averaged Navier-Stokes 82 equations in conjunction with the Reynolds-averaged Navier-Stokes (RANS)-based turbulence model [32], which 83 includes source terms for the effects of the dispersed phase on gas-phase turbulence. The turbulence combustion 84 interaction modeling (TCI) was not considered in the present study. As discussed by Pomraning et al. [33], 85 appropriate TCI models will reveal more small-scale details of flame structure compared to the well-mixed 86 models. However, such models are much more computationally expensive when implemented with detailed 87 mechanisms in engine-type simulations. On the other hand, the well-mixed models have been shown to be 88 accurate enough for predicting the basic two-phase flow properties, i.e., spray and vapor penetration, temperature 89 profile, ignition delay, and flame lift-off length, etc. Moreover, previous studies have demonstrated the validity of 90 such models for predicting combustion processes in both gasoline and compression ignition engines [26]. In 91 particular, Pomraning et al. [33] have provided a detailed assessment of the unsteady RANS-based approach, and 92 demonstrated that for well-resolved computations, the effects of mixing are accounted for using the RANS 93 turbulence model. Further improvements in the simulation results by implementing an appropriate TCI model will 94 be pursued in future work.

A finite volume methodology with a semi-implicit hybrid scheme is used to solve the governing equations on the Eulerian grid for the gas-phase properties, which include 3 velocity components, temperature, pressure, and species concentrations. The length and time scales associated with spray processes are too small to be resolved computationally, necessitating the use of sub-grid scale models to describe the spray physics. The spray is

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99 represented by a stochastic system of a discrete number of parcels, which are tracked computationally using a 100 Lagrangian scheme. The two phases are coupled through the mass, momentum, and energy exchange terms, 101 which are present in both the liquid- and gas-phase equations. The droplet breakup processes are modeled using 102 the Kelvin–Helmholtz and Rayleigh–Taylor (KH–RT) models [34]. Droplet collisions are modeled with the no 103 time counter algorithm [35]. A dynamic drag model [36] is used; it is based on the postulation that the drag 104 coefficient depends on the shape of the droplet, which can vary between a sphere and a disk. A droplet 105 evaporation model based on the Frossling correlation is used. Selected physical properties of n-heptane and 1-106 heptene fuels at 20°C and 1atm are listed in Table 1 [37]. As indicated, the difference between the physical 107 properties of the two fuels is not significant. Moreover, since the focus here is on the chemistry effects of fuel 108 unsaturation, simulations for both fuels are carried out using the physical properties of n-heptane. The effects of 109 turbulence on the droplet are accounted for by using a turbulent dispersion model. Detailed kinetic modeling is 110 performed by using the SAGE chemical kinetic solver [5] in CONVERGE, which is directly coupled with the 111 gas-phase calculations through a well-stirred reactor model.

The CFD solver uses an innovative modified cut-cell Cartesian method for grid generation [38]. The adaptive mesh resolution (AMR) technique enables local mesh refinement in regions of high curvatures. For the results presented here, the base (largest) grid size is fixed at 2mm. In order to resolve the flow near the injector, a local refinement area with 0.125mm grid sizes are used, along with AMR based on the curvature in the velocity and temperature fields. As discussed in the next section, these grid sizes were found to be sufficient to capture the spray droplet break up, vaporization and combustion processes.

118 **3. Reduced Mechanism Generation and Validation**

In order to perform well-resolved simulations for both n-heptane and 1-heptene spray flames at diesel engine conditions, a skeletal or reduced CRECK mechanism was developed to model the oxidation chemistry of these two fuels, and the NO_x and PAH formation. The skeletal mechanism (207 species and 4094 reactions) was obtained by reducing it from the detailed CRECK mechanism, based on the Directed Relation Graph with Error Propagation and Sensitivity Analysis (DRGEPSA) [28, 29]. The detailed CRECK mechanism (482 species and 124 19072 reactions), which has been developed and validated by Ranzi et al. [39, 40, 41, 42] for the simulations of
both low- and high-temperature combustion phenomena.

126 The DRGEPSA algorithm consists of two phases: (1) directed relation graph error propagation (DRGEP), 127 and (2) sensitivity analysis (SA). The mechanism reduction procedure has been reported by Lu and Law [28]. 128 Since it is difficult to identify and eliminate an unimportant species because of the coupling between species, the 129 following rule is employed to determine whether a species can be removed. Considering that species A directly 130 forms species B, the species B can be removed if and only if its removal will not induce a significant error in the 131 production rate of species A. This error is determined by a normalized contribution of reaction $A \rightarrow B$ among all 132 the reactions dependent on species A. Also key species are specified to keep certain important reaction routes 133 such as the detailed PAH and NO_x formation routes. In the present study, CH₃, acetylene (C_2H_2), benzene (C_6H_6), 134 pyrene ($C_{16}H_{10}$), ethylene ($C_{2}H_{4}$), propargyl ($C_{3}H_{3}$), cyclopentadiene ($c_{Y}C_{5}H_{6}$), naphthalene ($C_{10}H_{8}$), styrene 135 $(C_6H_5C_2H_3)$, NO, N₂O, NNH, CH, CO, OH, HO₂, H₂O₂ and heptylhydroperoxy (NC₇-QOOH) species are 136 specified to be kept in order to accurately account for the C1-C4 oxidation chemistry, n-heptane and 1-heptane 137 ignition behavior, and NO_x and PAH formation routes. The resulting reduced mechanism also contains all those 138 species that are related to the above key species. Once the optimal mechanism is obtained from the DRGEP step, 139 sensitivity analysis is performed to further reduce the size of the mechanism. All the species after DRGEP step are 140 arranged in ascending order based on the error in ignition delay induced by removing this species. The sensitivity 141 analysis removes the species identified from the top of the list one by one until the error generated by the resulting 142 skeletal mechanism with the remaining species reaches the user-defined tolerance for ignition delay.

The operating conditions used during the reduction and testing of the reduced mechanism include pressures of 30, 40, 50 atm, temperatures of 800, 900, 1000, 1100, 1200 K, and equivalence ratios of 0.5, 1.0, 1.5, 2. Fuels used include 100% n-heptane, 100% 1-heptene, 100% methane, 50%n-heptane/50%methane, 50%1-heptene/50%methane, 90%n-heptane/10%methane, and 90%1-heptene/10%methane by volume.

148 **3.1 Validation Using the Ignition and Spray Data from Experiments**

149 The reduced CRECK mechanism was validated against the shock tube ignition data for n-heptane and 1-150 heptene, as well as the non-reacting and reacting spray data from ECN. Figure 1a presents a comparison of the 151 predicted ignition delays against the measurements of Gauthier et al. [43] for n-heptane/air mixtures. Simulations 152 were performed in constant-pressure, homogeneous reactor using the CHEMKIN software and four different 153 mechanisms, namely, the reduced CRECK mechanism, Chalmers mechanism [44, 45], detailed CRECK 154 mechanism, and detailed Lawrence Livermore National Laboratory (LLNL) mechanism [46]. Overall, there is 155 good agreement between the various predictions and measurements. At high temperatures (T>1100 K), all the 156 four mechanisms overpredict ignition delays. However, at lower temperatures, relevant for ignition in diesel 157 engines, there is reasonably good agreement. Moreover, the reduced mechanism reproduces the experimentally 158 observed negative temperature coefficient (NTC) regime, wherein the ignition delay increases with temperature. 159 Figure 1b compares the ignition delays for 1-heptene/air mixtures predicted using the reduced and detailed 160 CRECK mechanisms against the measurements of Garner et al. [16]. Both the mechanisms are able to reproduce 161 the experimental data, although the values are somewhat overpredicted. Note that due to limited experimental 162 data, simulations only considered temperatures greater than 1300K. Moreover, for temperatures below 1300, the 163 ignition delays for 1-heptene become significantly higher compared to those for n-heptane.

164 Further validation of the reaction mechanism and spray models was performed using the high-fidelity 165 experimental data from the ECN [26] for turbulent non-reacting and reacting sprays. Validation for the non-166 reacting spray is useful as it establishes that the spray models accurately predict the spray development and 167 fuel-air distribution. A schematic of the combustion vessel used in experimental studies at Sandia can be 168 found in Refs. [26]. A cubical geometry of 108 mm on each side is used to represent the vessel geometry 169 in simulations. The vessel has a common-rail fuel injector that is mounted in a metal side-port such that 170 the spray is directed into the center of the chamber. The well-characterized engine relevant (high 171 temperature and pressure) initial conditions are created by burning a premixed fuel-air mixture. For 172 spray experiments, a range of ambient conditions in terms of density, temperature, and oxygen 173 concentrations can be provided. Further details of the vessel and injector are provided in Refs. [23, 47]. 174 For the results presented here, the base grid size is 2mm except for the grid convergence cases. In order to

resolve the flow near the injector, a fixed grid embedding is employed such that the minimum grid size is 0.125mm. In other regions, four levels of adaptive mesh refinement are employed based on the velocity and temperature fields. The simulations are performed on the High Performance Computing Cluster at UIC using up to three nodes. Each node has an Intel® Xeon® CPU at 2.60GHz with 16 cores and 20MB cache.

179 Figure 2 presents the liquid and vapor penetrations versus time for n-heptane non-reacting spray. 180 Predictions for the three grid sizes are compared with measurements. The experimental conditions used in the 181 simulations are listed in Table 2. Simulations use the same injection rate profile as experiments. The liquid 182 penetration distance is determined using the axial distance encompassing 97% of injected liquid n-heptane mass, 183 while the vapor penetration is calculated based on a fuel vapor mass fraction contour level of 1%. As indicated in 184 Fig. 3, the predicted liquid and spray penetrations are generally in good agreement with measurements. The liquid 185 penetration increases with time, and then stabilizes to a quasi-steady value. While the qualitative trends are 186 captured with all the three grid sizes, the quantitative agreement improves as the grid size is reduced, except for 187 the initial liquid penetration (for time below 0.5ms), which is overpredicted by the model. As discussed by Som et 188 al. [48], such differences may be attributed to several factors, including experimental uncertainties in near-nozzle 189 measurements, under-resolution of flow in the near-nozzle region, and inability to capture the effect of cavitation 190 and turbulence in the injector flow. It is also important to note that the predicted results are fairly grid-191 independent for the grid sizes of 0.25 and 0.125mm, and the spray development and vaporization processes are 192 fairly well resolved using the RNG k- ε turbulence model with the minimum grid size of 0.125mm. These results 193 are consistent with previous studies concerning grid convergence. Som et al. [48] performed computations of non-194 reacting and reacting sprays for n-heptane and n-dodecane fuels, and observed good agreement between 195 measurements and predictions using the RNG k-ɛ turbulence model with minimum grid size of 0.25mm. Xue et al. 196 [49] also performed simulations for the same two fuels using the RANS and LES turbulence models, and reported 197 grid convergence with grid sizes of 0.25mm and 0.125mm. Thus, the simulations in the present study were 198 performed using the minimum grid size of 0.125mm and four levels of adaptive mesh refinement (AMR) based 199 on the velocity and temperature fields, but a fixed grid embedding near the nozzle.

200 Validation results for the n-heptane reacting spray are presented in Figure 3, which compares the 201 measured and predicted ignition delays (τ_{ig}) and flame LOL for different initial temperatures. Additional validation for the predicted τ_{ig} and LOL for different O₂ concentrations is provided in Ref. [50]. The experimental 202 203 conditions used in the simulations are listed in Table 2. In experiments, τ_{ig} was determined using a criterion 204 based on a specific pressure rise, while in simulations, it was computed by using the time from start of 205 injection (SOI) to the instant when the maximum temperature (T_{max}) in the computational domain 206 exceeds a specified value (1500K). Using a different criterion based on the rate of change of T_{max} reaching a 207 peak value yielded essentially the same ignition delay. A specific OH mass fraction contour corresponding 208 to 2% of the peak value was used to determine the LOL in simulations, while it was measured using an 209 intensified CCD camera with a 310nm band-pass filter (10 nm FWHM) [51,52] in experiments. There is 210 fairly good agreement between the predictions and experimental data. Both the experiments and predictions 211 indicate a decrease in ignition delay, and consequently in LOL, as the initial temperature is increased. It is also 212 important to note that both simulations and measurements do not indicate the existence of NTC region, which can 213 be seen in Fig. 1a for homogeneous n-heptane/air mixtures. This may be related to the temporally and spatially 214 evolving temperature and species fields for the spray case [53].

215 Figure 4 compares the high speed soot luminosity images from ECN experiments with the soot contours 216 predicted using the RANS and LES models. The two-step soot model used in simulations is adopted from 217 Hiroyasu and Kadota [54]. The model assumes spherical particles formed by acetylene and, thus provides a 218 qualitative comparison with luminosity images. Note that while a two-step soot model based on acetylene is used 219 in the present study, the formation of PAHs is investigated in detail. The spray in the computed images (Fig. 4) is 220 shown by blue dots representing the size of liquid parcels, while the green contour line represents the OH mass 221 fraction contour corresponding to 2% of the peak value, and shows the flame envelope. Overall, there is good 222 agreement between the computed and measured flame images. As expected, the LES model provides more spatial 223 details or small-scale features compared to the RANS model. There is also good agreement between the measured 224 and predicted LOL values. Solid vertical lines at 0.017m in the computed images indicate the measured LOL.

225 4. N-Heptane Spray Flame Structure

Results here focus on the computed structure and emission characteristics of n-heptane and 1-heptene spray flames in the Sandia combustor. Figure 5 shows the temporal evolution of n-heptane spray flame in terms of temperature and mixture fraction contours at different times after the start of injection (SOI) for 1000K initial temperature and 21% O_2 . The black lines represent the mixture fraction or equivalence ratio ϕ ranging from 0.15 to 3, with ϕ defined as:

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$$\phi = \frac{2\sum_{i} N_{i} \eta_{C,i} + \frac{1}{2} \sum_{i} N_{i} \eta_{H,i}}{\sum_{i} N_{i} \eta_{O,i}}$$
(1)

Here *i* represents all species except CO₂ and H₂O, N_i the number of moles of species *i* and $\eta_{C,i}$, $\eta_{H,i}$ and $\eta_{O,i}$ the number of carbon (C), hydrogen (H) and oxygen (O) atoms, respectively, in *i*th species. The ϕ contours are good marker of the reaction zones. Only the center part (0.04x0.08m²) of the computational domain (0.108x0.108m²) is shown in the figure. The injector exit is located at the left boundary.

236 The processes of fuel injection, spray development, fuel-air mixing and ignition can be discerned from the 237 contour plots at 0.3 and 0.5ms. For instance, region within $\phi=3$ contour at 0.3ms indicates a fuel-rich zone 238 characterized by pre-ignition pyrolysis and oxidation reactions. Subsequently, the ignition occurs at 0.5ms, as 239 indicated by the high-temperature region between x=30mm and x=40mm. Note that the measured ignition delay 240 time in Sandia experiments for the same conditions was 0.53ms. The ignition process is more clearly depicted in 241 Fig. 6, which presents the heat release rate (HRR) contours (left) and scatter plots in ϕ -T space (right) at three 242 different times. Such scatter plots have previously been used to visualize the soot and NO_x formation regions in 243 IC engines, and also to provide insight into the ignition process [53]. The blue contours and scatter plots in Fig. 6 244 depict regions of negative HRR, indicating pre-ignition endothermic reactions. Moreover, prior to ignition event (at t=0.4ms), the peak HRR is only 1011J/s-m³, and located at T \approx 900K and $\phi \approx$ 4 in the scatter plot at t=0.4ms. 245 246 However, at t=0.5ms, a small region of high HRR can be visualized in the ϕ -T plot near ϕ =2.5 and T=1200K, 247 indicating the occurrence of ignition. Subsequently, a wide region with significant heat generation can be seen in

both the contour and scatter plots at 0.6ms, indicating self-sustained combustion with T>1200K and 0.1< ϕ <5. The combustion process is more clearly indicated in Fig. 5 by the ϕ and T contours at t=0.7 and 1.1ms. It is characterized by distinct regions of rich premixed combustion and diffusion combustion. For the present case, the rich premixed zone (RPZ) is indicated by region corresponding to 2< ϕ <5 and 2000K<T<2500, while the diffusion or non-premixed zone (NPZ) corresponds to 0.15< ϕ <2.5 and high temperatures (2500K<T<2800) due to exothermic reactions forming CO₂ and H₂O species. The green vertical lines at x=17mm in Fig. 5 mark the measured flame LOL, which matches with the predicted LOL indicated by the contours at t=0.7 and 1.1ms.

255 Figure 7 presents the integrated fuel vapor mass and HRR profiles with respect to time. The two-stage 256 ignition process can be clearly seen from the HRR profile. The first increase in HRR at 0.2ms is related to the 1st-257 stage ignition while the second sharp increase at 0.5ms pertains to the 2nd-stage ignition, followed by the rich 258 premixed combustion and the diffusion combustion. The rich premixed combustion is also indicated by the sharp 259 decrease in n-heptane mass between 0.5 and 0.8ms, while the diffusion combustion is indicated by more moderate 260 and nearly constant rate of decrease of n-heptane mass. The RPZ and NPZ can be distinguished more clearly in 261 Fig. 8, which presents C_2H_2 , OH, NO, and C_6H_6 mass fraction contours. As indicated, the RPZ and NPZ are 262 characterized, respectively, by the high concentrations of C₂H₂ and OH species. In addition, most of NO is formed 263 in the NPZ where temperatures are high, while benzene (C_6H_6) is formed in the RPZ.

264 In order to identify the relative contributions of various NO_x (NO and NO₂) formation routes, Figure 9 265 presents contour plots for the mass fractions of NO, NO₂, HCN, NH, N₂O and NNH. Note that HCN and NH 266 species are important for prompt NO, while N₂O and NNH species are associated with NO formed through the 267 N₂O intermediate and NNH intermediate routes, respectively. As can be seen in Fig. 9a, most of NO is formed in 268 NPZ, with a relatively a small amount also being formed in RPZ and the region outside NPZ. The NO formed in 269 NPZ is predominantly through the thermal NO route since temperatures are the highest (2600K to 2900K) there. 270 In indicated in Fig. 9b, most of NO_2 is formed in the region outside NPZ, where temperature is about 1500K and 271 abundant amount of O₂ is present. The prompt NO is mainly formed in RPZ as indicated by the HCN and NH 272 contours in Figs. 9c and 9d, respectively. Finally, N₂O is formed in the lean region outside the NPZ similar to

NO₂, (cf. Fig. 9e), while NNH is formed in the region between the RPZ and NPZ (cf. Fig. 9f), implying that NNH
intermediate route is important there.

275 4.1 Effect of Fuel Molecular Structure on NO and PAH Formation

276 In order to characterize the effect of fuel molecular structure or unsaturation on NO and PAH emissions, 277 n-heptane and 1-heptane spray flames were simulated at identical conditions in the Sandia reactor. Figure 10 278 presents the temporal variations of peak temperature and integrated NO mass for the two flames. Note that at 279 typical autoignition temperatures (800-1000K) in diesel engines, 1-heptene has much longer ignition delays than 280 n-heptane. Consequently, simulations were performed with an initial temperature of 1300K. At this temperature, 281 ignition delays for the two fuels are nearly the same (≈ 0.2 ms), as indicated in Fig. 10. These values also compare 282 well with the measured value of 0.26ms in Sandia experiments. More importantly, the peak temperature for 1-283 heptene flame is 2870K compared to a value of 2840K for n-heptane flame. Consequently, 1-heptene flame 284 produces more NO compared to n-heptane flame. For example, at t=1.4ms, the total NO in 1-heptane flame is 18% 285 higher than that in n-heptane flames, and the difference can be mostly attributed to increased thermal NO in 1-286 heptene flame.

287 Since temperature is the important factor for thermal NO, the increased NO in 1-heptene flame can be 288 attributed to higher peak temperature in this flame. Note that the heating value of 1-heptene is (LHV=44.66MJ/kg) 289 is slightly lower than that of n-heptane (44.92MJ/kg). Thus the higher peak temperature in 1-heptene flame is not 290 related to the heating value, but to the fuel oxidation chemistry. In order to examine this aspect, homogeneous 291 reactor simulations were performed at similar conditions. Figure 11 presents the reaction path analysis for the two 292 fuels, based on constant volume simulations with initial conditions similar to those for spray flames, i.e., 293 T=1300K, p=55atm, ϕ =1. At these conditions, oxidation routes are significantly different for the two fuels. As 294 indicated in Fig. 11a, the dominant path for n-heptane is through H abstraction reaction forming alkyl radicals. 295 Here the more prominent reaction is C_7H_{16} + OH=> H₂O+C₇H₁₅. A relatively small amount of n-heptane (12%) 296 also decomposes through the breaking of C-C bonds to form smaller alkyl radicals with 2 to 5 carbons. 297 Subsequently, about 82% of C_7H_{15} undergoes β scission reactions forming smaller ($C_2 \sim C_5$) alkyls and olefins,

while about 12% of C_7H_{15} undergoes oxidation with O_2 and isomerization to form heptyl-hydroperoxy radical (C_7H_{14} -QOOH). However, the heptyl-hydroperoxy radicals directly dissociate into small hydrocarbons and heptene (C_7H_{14}), and the latter gets oxidized to form $C_2\sim C_5$. In contrast, due to the presence of double bond, about 33% of 1-heptene undergoes β scission reactions, mainly though reactions C_7H_{14} +OH=>CH₂CHCH₂+C₄H₈+H₂O and C_7H_{14} =>CH₂CHCH₂+C₄H₉, to form allyl radicals (CH₂CHCH₂). The rest 67% of 1-heptene is oxidized to form smaller hydrocarbons. All these oxidation reactions are faster compared to the dissociation reaction of 1heptene. Consequently, the ignition delay is shorter for 1-heptene compared to that of n-heptane.

305 Figure 12 compares the temporal profiles of temperature and NO mole fraction for the two fuels. These 306 simulations were performed in a well-stirred reactor using the Chemkin software. Consistent with the reaction 307 path analysis, the ignition delay times are 0.014ms and 0.018ms, while the peak temperatures are 3241K and 308 3217K for 1-heptene and n-heptane, respectively. The higher temperature is responsible for the 6.1% higher in 309 NO for 1-heptene compared to that for n-heptane. Similar differences are observed for the NO formed through the 310 prompt, N₂O and NNH intermediate routes for the two fuels. Figure 13 compares the total amounts of HCN, N₂O, 311 NNH, and CH species in n-heptane and 1-heptane flames at 1.4ms. The CH₂ plot is similar to CH plot, and not 312 shown. The amounts of HCN, N₂O, and NNH are higher in 1-heptene flame compared to those in n-heptane flame, 313 indicating that the NO formed through these routes is also higher in 1-heptene flame. Amongst the three routes, 314 the contribution of prompt NO is more significant compared to the N_2O and NNH intermediate routes. This is 315 based on the fact that the total mass of HCN is noticeably higher than those of N_2O and NNH. It is also important 316 to note that the amounts of CH and CH₂ (not shown) produced in n-heptane and 1-heptane flames are similar, 317 implying that the prompt NO route depends less on these species, and more on the higher temperature in 1-318 heptene flame. Figure 14 presents the scatter plots of HCN, N₂O and NNH in ϕ -T space for the n-heptane and 1-319 heptene flames. Consistent with the plots of these species in Fig. 9, most of HCN and thus prompt NO is formed 320 in RPZ, i.e., in the region $2 \le 4 \le 6$ and $1700 \le T \le 2200$, while N₂O is formed in the lean region outside NPZ with 321 1500<T<2000, and NNH is formed between RPZ and NPZ, in the region 2< ϕ <3 and 2400<T<2700. 322 Quantitatively, 1-heptene produces significantly higher HCN and thus higher prompt NO compared to that of nheptane, as indicated by a wider range of red dots. The contributions of N_2O and NNH intermediate routes are also higher in -1-heptene flame that those in n-heptane flame, but the differences are not as significant.

325 Figure 15 presents the benzene mass fraction contours for 1-heptene and n-heptane flames at t=1.4ms. 326 While the benzene formation region is located within the rich premixed zone for both flames, the amount of 327 benzene formed in 1-heptene is significantly higher. The peak mass fractions are 0.0118 and 0.0087 for 1-heptene 328 and n-heptane, respectively, i.e., 36% higher benzene for 1-heptene. Similar trends were observed for the 329 formation of heavier PAH, such as pyrene ($C_{16}H_{10}$). Figure 16 compares the temporal variation of integrated mass 330 of benzene and pyrene in n-heptane and 1-heptene flames. As expected, 1-heptene flame produces significantly 331 more benzene and pyrene compared to n-heptane flame, with the differences being 22.0% and 21.9% for benzene 332 and pyrene, respectively, at t=1.4ms.

333 Since benzene is an important aromatic species for pyrene and subsequent soot formation, it is important 334 to identify the dominant path for benzene formation. The path analysis is presented in Fig. 17, based on well-335 stirred reactor simulations for the combustion of the two fuels at the same conditions as those of Fig. 11. Two 336 major routes to form benzene involve reactions methyl-cyclo-pentadiene (MCPTD)=>benzene and 337 C_3+C_3 =>benzene, where C_3+C_3 represent reactions involving either two propargyl (C_3H_3) radicals or a propargyl 338 reacting with allene (AC₃H₄) or propyne (PC₃H₄). While these two routes appear to be similar for the two fuels, 339 the amount of benzene formed is higher in 1-heptene due to the higher concentrations of allene and C_4H_5 species. 340 This is due to the fact that the presence of double bond in 1-heptene opens an additional route (highlighted with 341 red) for allene formation through 1,3-butadiene (C_4H_6) and 3-butenal (C_3H_5CHO). In addition, the contribution of 342 C_4H_5 route to form allene in 1-heptene is increased to 14% compared to 8% for n-heptane. Since these two routes 343 are both associated with 1,3-butadiene, further analysis was done to identify the reason for the increased 344 formation of 1,3-butadiene in 1-heptene. As highlighted by red lines in Fig. 17, this can be attributed to the 345 presence of double bond in 1-heptene, which leads to its direct decomposition to form two C_4 hydrocarbons, C_4H_8 346 and CH₂C₃H₅, through β scission reaction. These two C₄ species lead to the formation of 1,3-butadiene and C₄H₇ 347 in 1-heptene. In contrast, there are fewer routes to form 1,3-butadiene and C_4H_7 in n-heptane. Moreover, the two 348 routes involving C_4H_8 and C_5H_{10} produce much less 1,3-butadiene compared to the direct decomposition reactions

349 for 1-heptene. Finally, 1-heptene also produces higher amount of cyC_5H_5 through C_5H_8 which further increases 350 the amount of benzene formed through methyl-cyclo-pentadiene route. Thus, while the relative contributions of 351 the two benzene formation routes are similar for the two fuels (21% for MCPTD route and 79% for C3 route vs. 352 20% and 80% for n-heptane and 1-heptane, respectively), the amount of benzene formed is higher in 1-heptane 353 due to the significantly higher amounts of 1,3-butadiene and allene. This is further confirmed in Fig. 18, which 354 compares the integrated amounts of acetylene, propargyl, 1,3-butadiene and allene formed in n-heptane and 1-355 heptene flames. While the amounts of acetylene and propargyl formed in the two flames are similar, significantly 356 higher amounts of 1,3-butadiene (about 117% higher) and allene (48% higher) are formed in 1-heptene flame 357 compared to those in n-heptane flame. Thus the pathway analysis based on well-stirred reactor simulations 358 confirm the 3-D CFD results that the increased amount of benzene in 1-heptene flame is associated with the β 359 scission reactions due to the presence of double bond in 1-heptene. This result is generally consistent, except for 360 the methyl-cyclo-pentadiene route, with the reaction path analysis for benzene formation reported in a previous 361 study [55] dealing with 1-heptene and n-heptane counterflow flames.

362 5. Conclusions

363 We have examined the effect of fuel unsaturation on NO_x and PAH formation in n-heptane and 1-heptene 364 spray flames at diesel engine conditions. The directed relation graph with error propagation and sensitivity 365 analysis has been employed to develop a reduced kinetic mechanism (with 207 species and 4094 reactions), 366 starting from the detailed CRECK mechanism [42] containing 482 species and 19072 reactions. The mechanism 367 and spray models have been validated against the shock tube ignition data and high-fidelity spray data in a 368 constant-volume combustion vessel from the Engine Combustion Network (ECN) [26]. The 3-D CONVERGE 369 software has been used to examine the structure and emission characteristics of n-heptane and 1-heptene spray 370 flames in the same vessel. Important observations are as follows.

(1) Validation of the reduced mechanism for the ignition of n-heptane/air and 1-heptene/air mixtures indicates
 fairly good agreement between the predictions and measurements. The mechanism also shows good
 agreement with other detailed and reduced mechanisms, and reproduces the experimentally observed negative

temperature coefficient (NTC) behavior for n-heptane/air mixtures. In addition, results indicate that at
moderate temperatures (800<T<1100), ignition delays for 1-heptene are significantly higher than those for n-
heptane, but similar at high temperatures. Validations of the 3-D simulations against the ECN data for nheptane sprays also show good agreement between the predicted and measured spray penetration lengths,
ignition delays, flame liftoff lengths, and global flame structure.

- 379 (2) Simulation results for n-heptane and 1-heptene spray flames indicate that the combustion under diesel engine 380 conditions is characterized by a double-flame structure with a rich premixed reaction zone (RPZ) near the 381 flame stabilization region and a non-premixed reaction zone (NPZ) further downstream. The RPZ and NPZ 382 are characterized, respectively, by the high concentrations of C_2H_2 and OH species.
- (3) The scatter plots in ϕ -T space are used to identify the dominant NO_x and PAH formation regions in spray flames. For the conditions investigated, most of NO_x is formed via thermal NO route in the NPZ, while PAH species are mainly formed in the RPZ. Relatively small amount of NO is also formed via prompt route in the RPZ, and via N₂O intermediate route in the fuel-lean region outside NPZ, and via NNH intermediate route in the region between RPZ and NPZ.

(4) The presence of a double bond leads to higher flame temperature and consequently higher thermal NO in 1heptene flame than that in n-heptane flame. It also leads to the significantly higher amounts of PAH species, implying higher soot emission in 1-heptene flame compared to that in n-heptane flame. Reaction path analysis indicates that this can be attributed to β scission reactions due to the presence of double bond, which lead to the significantly higher amounts of 1,3-butadiene and allene formed in 1-heptene compared to those in nheptane. Moreover, the presence of double bond in 1-heptene opens an additional route for allene formation through 1,3-butadiene (C₄H₆) and 3-butenal (C₃H₅CHO) species.

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399 **6. Reference**

- [1] Mehl M, Vanhove G, Pitz WJ, Ranzi E. Oxidation and combustion of the n-hexene isomers: a wide range kinetic modeling study. Combust. Flame. 2008; 155: 756–772.
- [2] Bounaceur R, Warth V, Sirjean B, Glaude PA, Fournet R, Battin-Leclerc F. Influence of the position of the double bond on the autoignition of linear alkenes at low temperature Proc. Combust. Inst. 2009; 32: 387– 394.
- [3] Westbrook CK, Pitz WJ, Sarathy SM, Mehl M. Detailed chemical kinetic modeling of the effects of CC double bonds on the ignition of biodiesel fuels. Proc. Combust. Inst. 2013; 34: 3049–3056.
- [4] Touchard S, Buda F, Dayma G, Glaude PA, Fournet R, Battin-Leclerc F. Experimental and modeling study of the oxidation of 1-pentene at high temperature. Int. J.Chem. Kinet 2005; 37: 451–463.
- [5] Mehl M, Pitz WJ, Westbrook CK, Yasunaga K, Conroy C, Curran HJ. Autoignition behavior of unsaturated hydrocarbons in the low and high temperature regions. Proc. Combust. Inst. 2011; 33: 201–208.
- [6] Garner S, Sivaramakrishnan R, Brezinsky K. The high pressure pyrolysis of saturated and unsaturated C7 hydrocarbons. Proc. Combust. Inst. 2009; 32: 461–467.
- [7] Minetti R, Roubaud A, Therssen E, Ribaucour M, Sochet LR. The chemistry of pre-ignition of n-pentane and 1-pentene. Combust. Flame. 1999; 118: 213–220.
- [8] Ribaucour M, Minetti R, Sochet LR. Autoignition of n-pentane and 1-pentene: experimental data and kinetic modeling. Proc. Combust. Inst. 1998; 27: 345–351.
- [9] Vanhove G, Ribaucour M, Minetti R. On the influence of the position of the double bond on the low-temperature chemistry of hexenes. Proc. Combust. Inst. 2005; 30: 1065–1072.
- [10] Prabhu SK, Bhat RK, Miller DL, Cernansky NP. 1-Pentene oxidation and its interaction with nitric oxide in the low and negative temperature coefficient regions. Combust. Flame. 1996; 104: 377.
- [11] Schönborn A, Ladommatos N, Williams J, Allan R, Rogerson J. The influence of molecular structure of fatty acid monoalkyl esters on diesel combustion. Combust. Flame. 2009; 156: 1396–1412.
- [12] Puhan S, Saravanan N, Nagarajan G, Vedaraman N. Effect of biodiesel unsaturated fatty acid on combustion characteristics of a DI compression ignition engine. Biomass Bioenergy. 2010; 34: 1079–1088.
- [13] Benjumea P, Agudelo JR, Agudelo AF. Effect of the degree of unsaturation of biodiesel fuels on engine performance, combustion characteristics, and emissions. Energy Fuels. 2011; 25: 77–85.
- [14] Lapuerta M, Herreros JM, Lyons LL, García-Contreras R, Briceño Y. Effect of the alcohol type used in the production of waste cooking oil biodiesel on diesel performance and emissions. Fuel. 2008; 87: 3161–3169.
- [15] Salamanca M, Mondragon F, Agudelo JR, Benjumea P, Santamaría A. Variations in the chemical composition and morphology of soot induced by the unsaturation degree of biodiesel and a biodiesel blend. Combust. Flame. 2012; 159: 1100–1108.
- [16] Garner S, Brezinsky K. Biologically derived diesel fuel and NO formation: An experimental and chemical kinetic study, Part 1. Combust. Flame. 2011; 158: 2289–2301.
- [17] Garner S, Dubois T, Togbe C, Chaumeix N, Dagaut P, Brezinsky K. Biologically derived diesel fuel and NO formation: Part 2: Model development and extended validation. Combust. Flame. 2011; 158: 2302– 2313.
- [18] Frenklach M, Wang H. Detailed modeling of soot particle nucleation and growth. Proc. Combust. Inst. 1991; 23: 1559.
- [19] Frenklach M. Reaction mechanism of soot formation in flames. Phys Chem. Chem. Phys. 2002; 4: 2028– 2037.
- [20] Sarathy SM, Gaïl S, Syed SA, Thomson MJ, Dagaut P. A counterflow diffusion flame study of lightly branched octane isomers. Proc. Combust. Inst. 2007; 31: 1015–1022.
- [21] Fu X, Garner S, Aggarwal SK, Brezinsky K. Numerical study of NOx emissions from n-Heptane and 1-Heptene counterflow flames. Energy Fuels. 2013; 27: 537–548.

- [22] Han X, Aggarwal SK, Brezinsky K. Effect of unsaturated bond on nox and pah formation in n-heptane and 1-heptene triple flames. Energy Fuels. 2012; 26: 879–888.
- [23] Idicheria CA, Pickett LM. Ignition, soot formation, and end-of-combustion transients in diesel combustion under high-EGR conditions. Int. J. Engine Research. 2011; 12: 376–392.
- [24] Pickett LM, Manin J, Genzale CL, Siebers DL, Musculus MPB, Idicheria CA. Relationship between diesel fuel spray vapor penetration/dispersion and local fuel mixture fraction. SAE International Journal of Engines 2011; 4: 764–799.
- [25] Pickett LM, Kook S, Williams TC. Visualization of diesel spray penetration, cool-flame, ignition, high-temperature combustion, and soot formation using high-speed imaging. SAE Paper 2009-01-0658.
- [26] Engine Combustion Network (ECN), diesel sprays data search utility. Accessed on Feb. 2015. (http://www.sandia.gov/ecn/cvdata/dsearch/frameset.php).
- [27] Ranzi E, Frassoldati A, Grana R, Cuoci A, Faravelli T, Kelley AP, Law CK. Hierarchical and comparative kinetic modeling of laminar flame speeds of hydrocarbon and oxygenated fuels. Prog. Energy Combust. Sci. 2012; 38: 468–501.
- [28] Lu TF, Law CK. A directed relation graph method for mechanism reduction. Proc. Combust. Inst. 2005; 30:1333–1341.
- [29] Raju M, Wang M, Senecal PK, Som S, Longman DE. A reduced diesel surrogate mechanism for compression ignition engine applications. Proceedings of the ASME 2012 Internal Combustion Engine Division Fall Technical Conference, Vancouver, BC, Canada, ICEF2012-92045, 2012.
- [30] Senecal PK, Pomraning E, Richards KJ. A study for measurement of oil film thickness on engine bearing by using laser induced fluorescence (LIF) method. SAE Paper 2003-01-0243.
- [31] Senecal PK, Richards KJ, Pomraning E, Yang T, Dai MZ, McDavid RM, Patterson MA, Hou S, Sethaji T. A new parallel cut-cell cartesian CFD code for rapid grid generation applied to in-cylinder diesel engine simulations. SAE Paper 2007-01-0159.
- [32] Han Z, Reitz RD.Turbulence Modeling of internal combustion engines using RNG κ-ε models. Combust. Sci. and Tech. 1995; 106: 267–295.
- [33] Pomraning E, Richards K, Senecal P. Modeling turbulent combustion using a RANS model, detailed chemistry, and adaptive mesh refinement. SAE Technical Paper 2014-01-1116.
- [34] Patterson MA, Reitz RD. Modeling the effects of fuel spray characteristics on diesel engine combustion and emission. SAE paper, 1998-980131.
- [35] Schmidt DP, Rutland CJ. A new droplet collision algorithm. J. Comput. Phys. 2000; 164: 62–80.
- [36] Liu AB, Mather DK, Reitz RD. Modeling the Effects of Drop Drag and Breakup on Fuel Sprays. SAE paper, 1993-930072.
- [37] PubChem Open Chemistry Database. (http://pubchem.ncbi.nlm.nih.gov/). Accessed on Feb. 2015.
- [38] Richards KJ, Senecal PK, Pomraning E. CONVERGE (Version 2.1.0), Convergent Science, Inc., Middleton, WI. 2013.
- [39] Cuoci A, Frassoldati A, Faravelli T, Ranzi E. Formation of soot and nitrogen oxides in unsteady counterflow diffusion flames. Combust. Flame. 2009; 156: 2010–2022.
- [40] Frassoldati A, Faravelli T, Ranzi E. Kinetic modeling of the interactions between NO and hydrocarbons at high temperature. Combust. Flame. 2003; 135: 97–112.
- [41] Faravelli T, Frassoldati A, Ranzi E. Kinetic modeling of the interactions between NO and hydrocarbons in the oxidation of hydrocarbons at low temperatures. Combust. Flame, 2003; 132: 188–207.
- [42] http://creckmodeling.chem.polimi.it/index.php/current-version-kinetic-mechanisms/low-and-high-temperature-complete-mechanism. Accessed on July 2014.
- [43] Gauthier BM, Davidson DF, Hanson RK. Shock tube determination of ignition delay times in full-blend and surrogate fuel mixtures. Combust. Flame. 2004; 139: 300–311.
- [44] http://www.tfd.chalmers.se/~valeri/MECH.html.
- [45] Tao F, Reitz RD, Foster DE. Revisit of diesel reference fuel (n-heptane) mechanism applied to multidimensional diesel ignition and combustion simulations. Proceedings of International Multidimensional Engine Modeling User's Group Meeting, Detroit, MI, April 15, 2007.

- [46] Curran HJ, Gaffuri P, Pitz W J, Westbrook C K. A comprehensive modeling study of n-heptane oxidation. Combust. Flame 1998; 114: 149–177.
- [47] Idicheria CA, Pickett, LM. Effect of EGR on diesel premixed-burn equivalence ratio. Proc. Combust. Inst. 2007; 31: 2931–2938.
- [48] Som, S, D'Errico, G, Longman, D, and Lucchini, T. Comparison and standardization of numerical approaches for the prediction of non-reacting and reacting diesel sprays. SAE Technical Paper 2012-01-1263.
- [49] Xue Q, Som S, Senecal P K, Pomraning E. Large eddy simulation of fuel-spray under non-reacting ic engine conditions. Atomization and Sprays, 2013; 23: 925–955.
- [50] Fu X, Partially premixed combustion in counterflow flame and dual fuel compression ignition engine, PhD Thesis, Department of Mechanical and Industrial Engineering, University of Illinois at Chicago, 2015.
- [51] Siebers DL, Higgins B. Flame lift-off on direct-injection diesel sprays under quiescent conditions. SAE Paper 2001-01-0530.
- [52] Higgins B, Siebers DL. Measurement of the flame lift-off location on DI diesel sprays using OH chemiluminescence. SAE Paper 2001-01-0918.
- [53] Fu X, Aggarwal S K. Two-stage ignition and NTC phenomenon in diesel engines. Fuel, 2015; 144: 188– 196.
- [54] Hiroyasu H, Kadota T. Models for combustion and formation of nitric oxide and soot in direct injection diesel engines. SAE Paper 1976-760129.
- [55] Fu X, Han X, Brezinsky K, Aggarwal S. Effect of fuel molecular structure and premixing on soot emissions from n-heptane and 1-heptene flames. Energy Fuels, 2013; 27: 6262–6272.